



Gas mixture in light-weight JSP bottle

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Why using premixed gases in JSP bottle? No need for gas mixing system on site

• Content 12.3 1

• Pressure up to 20 bar gauge

- Useful for small flows (like 0.1 1.0 l/h)
 - \blacksquare => running time 10 100 days
- Relaxed safety requirements
 - When filled with flammable mixture less dangerous than a simple spray can
 - Possibly may be placed in test beam area
 - => short and thin pipes, low dead volume
- Using premixed from commercial vendors not attractive
 - Expensive
 - Long delivery time (5 6 weeks)

=> We built a gas filling system in house (Nikhef)



Gas bottle

Empty weight 4.1 kg

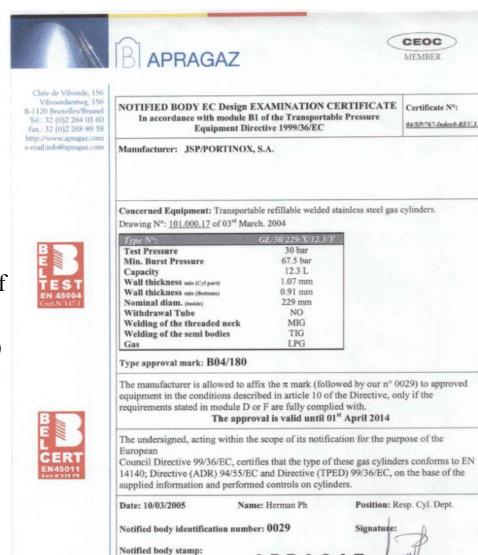
- Volume: 12.3 1
- Special version of light weight bottle
 - Fabricate JSP
 - Originally intended for butane and propane
- Material: AISI 304 (stainless steel)
- Test pressure: 30 bar
- Burst pressure: 140 bar
 - Controlled burst location (cylinder bottom)
- Equipped with safety valve opening at 27 bar gauge
 - => good filling pressure: 20 bar gauge
- Seals of outlet valve and safety valve: NBR (nitrile)
 - Outlet valve: only gas exposure to metals when closed
- Valve thread for regulator: LU-1 (W21,8x1/14"L)
 - (commonly used left thread for flammable gases)





Certificates

- 🔶 TPED 1999/36 (pi)
- ♦ EN14140
- ADR (international transport of dangerous goods by rail)
- RID (international transport of dangerous goods by train)
- IMDG (international marine code of dangerous goods)
- RRP (pressure container regulation)
- RAP (pressure machine regulation)
- Certified to conform to EN 14140; Directive (ADR) 94/55/EC and Directive (TPED) 99/36/EC
- All certificates apply for bottle filled with liquefied flammable gas
 - LPG, Butane, Propane



Notified body reference: 0405/B.0165

RAGAZ

Belaium

Inspecting

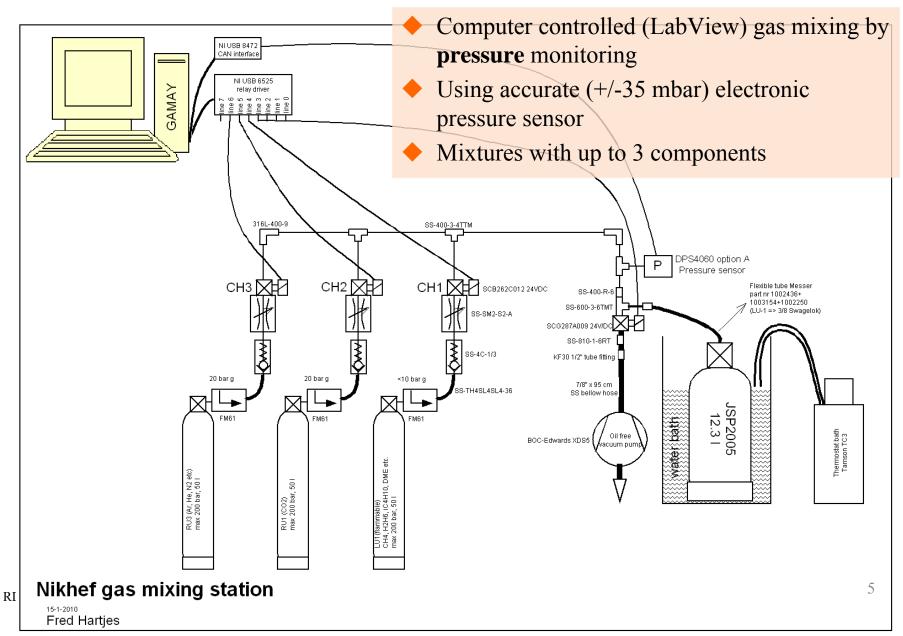
Authority



Eng. Ph. HERMAN

Cylinders Dept. Head

Diagram Nikhef gas filling system



Planned filling sequence

- 1. Put required mixture in LabView sequencer
 - Partial pressures will be calculated
- 2. Evacuate bottle and tubing to < 1 mbar
- 3. Fill to ~ 1 bar abs with "background" gas (argon, CO2, He, N2,)
- 4. Re-evacuate
- 5. Fill with component 1 to desired partial pressure and stop automatically
- 6. Measure obtained pressure after few minutes
- 7. Add component 2 to desired summed pressure and stop automatically
- 8. Measure obtained pressure
- 9. Even so for component 3
- 10. Calculate obtained mixing ratio
- 11. Print bottle label and write data in log file

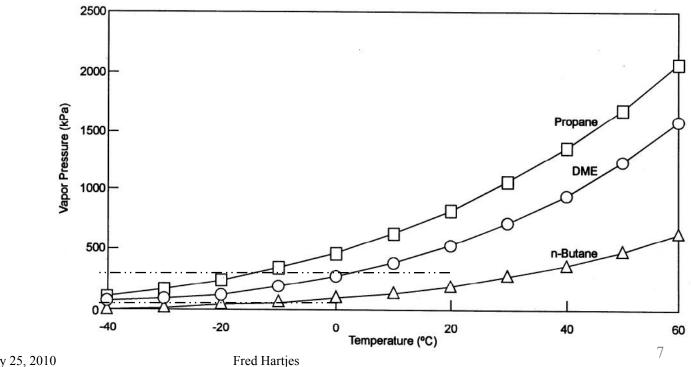




Vapour pressures vs temperature

Maximum bottle pressure often determined by condensation point

- Isobutane 2.6 bar @ 15 °C
 - \blacksquare => Ar/iC₄H₁₀ 50/50 can be no more than 5.2 bar abs or **4.2 bar gauge**
- DME 5.1 bar @ 20 °C
 - Boiling point 24.8 °C



Expected performance

- Accuracy of the component fraction 0.1% of total mixture
- Deviation from required mixture 1% of total mixture
- Example:
 - Target mixture Ar/CH 90/10
 - Realized mixture will be something like $Ar/CH_4(90.08\pm0.1)/(9.92\pm0.1)$
- Contamination
 - O_2 , N_2 , H_2O on ppM level
 - To be confirmed
- There will be no independent analysis of the mixture or to traces of contamination
 - Measuring oxygen on ppM level might be possible

Possible contamination by materials filling system

- ♦ Gas bottle
 - Stainless steel AISI 304
- Valves
 - NBR
 - Teflon tape
 - Piping, fittings
 - stainless steel
- Cleaning
 - Piping, fittings: well cleaned
 - Gas bottle
 - Etched, flushed and neutralised after high temperature manufacturing
 - Baking out not standard but possible (130 °C under vacuum)
 - High temperature baking (300 800 °C possible when dismantling valve

=> for critical operation adequate filtering (molecular sieve) mandatory
ageing tests



Security rules for the gas mixing station at Nikhef

• Creating mixtures with flammable gases at Nikhef allowed if

- Done in well vented space
- Explosion detection available
- Proper grounding of equipment
- Only accessible for limited number of persons
- These persons are well trained
- Additional fire extinguisher is present
- Risk analysis has been made
- Flammable gas indication is outside
- Security staff has been informed and instructed

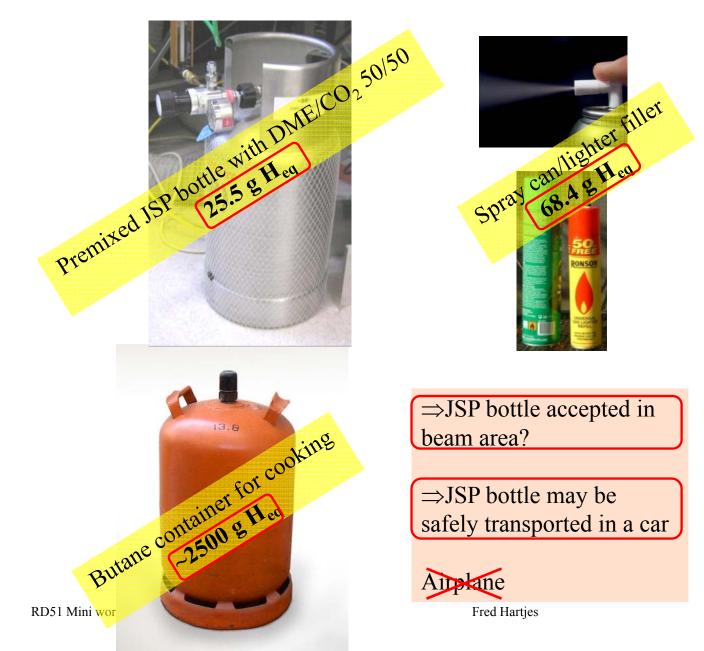
Using JSP bottle with flammable gas mixtures at a CERN test beam

Pressure of DME and isobutane mixtures limited by vapour pressure



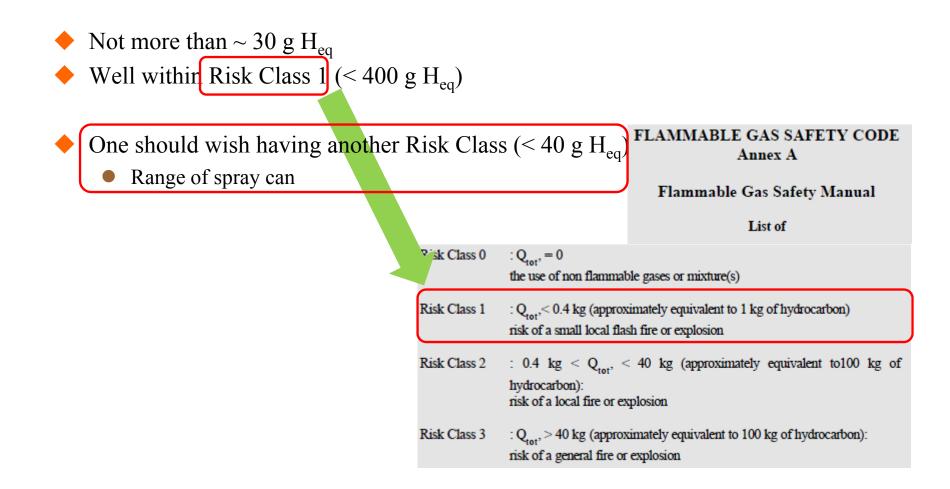
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Mixture	P1 (bar abs)	P2 (bar abs)	P _{tot} (bar gauge)	Net content (l)	H ₂ eq. mass(g)	Running time (days) at 0.3 l/h	
Ar/CH ₄ 90/10	18.9	2.1	20	246	7.0	33.2	
CO ₂ /DME 50/50	4.0	4.0	7.0	86	25.4	12.0	
Ar/iC ₄ H ₁₀ 80/20	8.8	2.2	10	123	26.0	17.1	

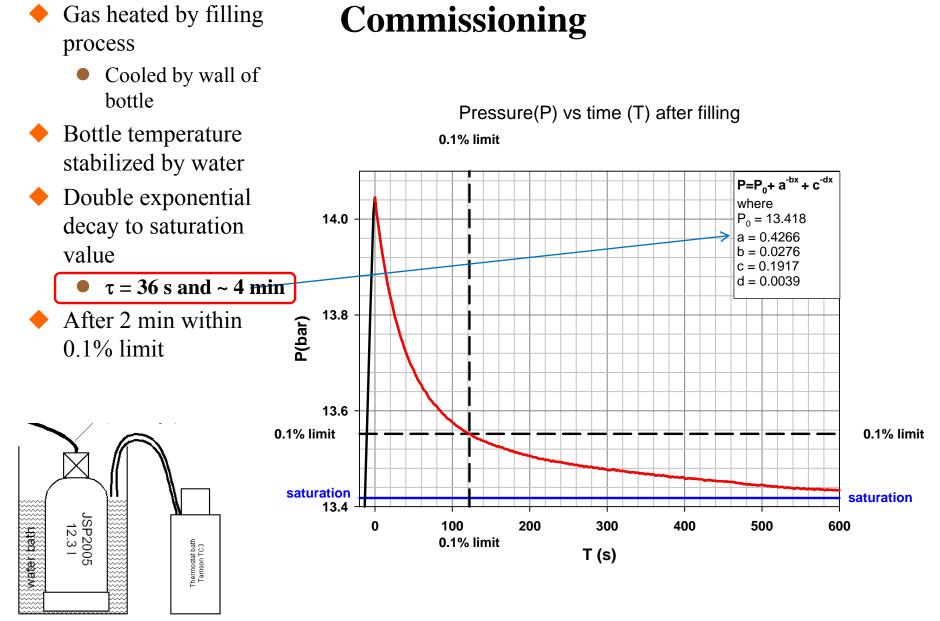
Safety in perspective





Using JSP bottles with flammable mixture at CERN





Present status 22-2-2010

+ Finished

- Hardware installation
- Remote control operational
 - Electromagnetic valves
 - Vacuum pump
 - Pressure meter

To be done

- Commissioning
- Operation program (LabView)
 - Sequencing
 - Logging
- CE certification



Conclusions

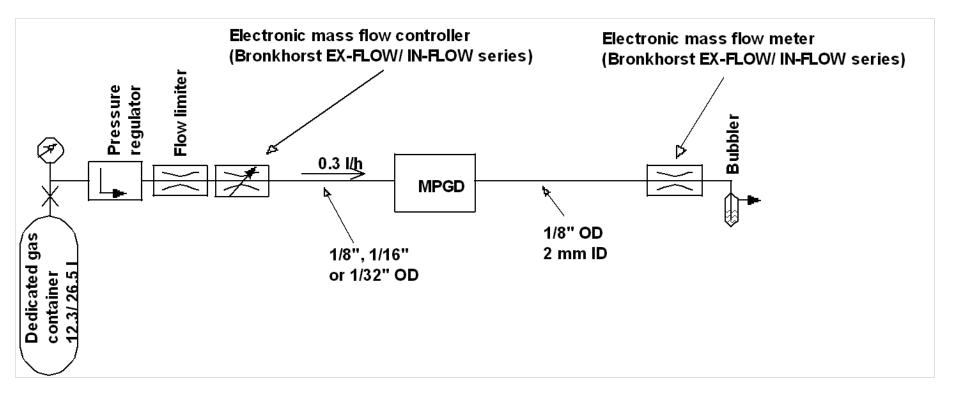
- Using premixed gases in JSP bottles has many advantages for low (< 1 l/h) flow applications
 - Thin gas pipes (1/8")
 - Premix gas bottles in lab/ test beam area
 - Simple, non critical (1 channel) gas regulation
 - Easy and cheap experimental set-up
- Nikhef installation will be soon ready to fill the JSP bottles



Spare

Test beam gas system with premixed bottles

- Assume small flow (≤ 0.3 l/h)
- Flow regulated by electronic mass flow controller (explosion proof)
- Flow check (electronic mass flow sensor) at exhaust
 - => verifying leaks
- Upstream: thin pipes may be used (1/8", 1/16", 1/32")
- Downstream: thicker pipes (1/8")



What is different for single chip MPGDs?

............

• Very small detector volumes

• 1 Gossip detector \approx **0.2 ml** (15 x 15 x 1 mm³)

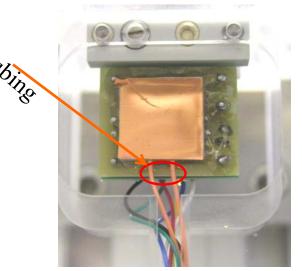
> very small gas flows may be used

- 10 volume changes/hour
- => 33 μ l/min (2 ml/h)
- Commercial mass flow controllers go down to ~ 2 ml/min FS
 - => permit flows down to 100 μ l/min
- For practical reasons we normally use bit larger flows
 - 2 5 ml/min (**0.12 0.3 l/h**)

Advantages of small flows (0.12 – 0.3 l/h)

1/32,

- Permitting very thin gas lines
 - Gas lines 1/32" ($\approx 0.8 \text{ mm OD}$) well feasible
 - **3** m tubing **0.5 mm ID** with CO_2 and 0.12 0.3 l/h
 - => Back pressure 10 24 mbar
 - Gas line of 1/64" ($\approx 0.4 \text{ mm OD}$) not excluded
 - **3** m tubing **0.25 mm ID** with CO_2 and 0.12 0.3 l/h
 - => Back pressure 0.15 0.4 bar



- (Using normal size gas pipes (6 mm OD or larger) would lead to very long reaction times)
- On site mixing of small flows hard
 - Long flow measurement times
 - (almost) out of range of commercial mass flow controllers
- => use premixed gas bottles